

Worldwide Pollution Control Association

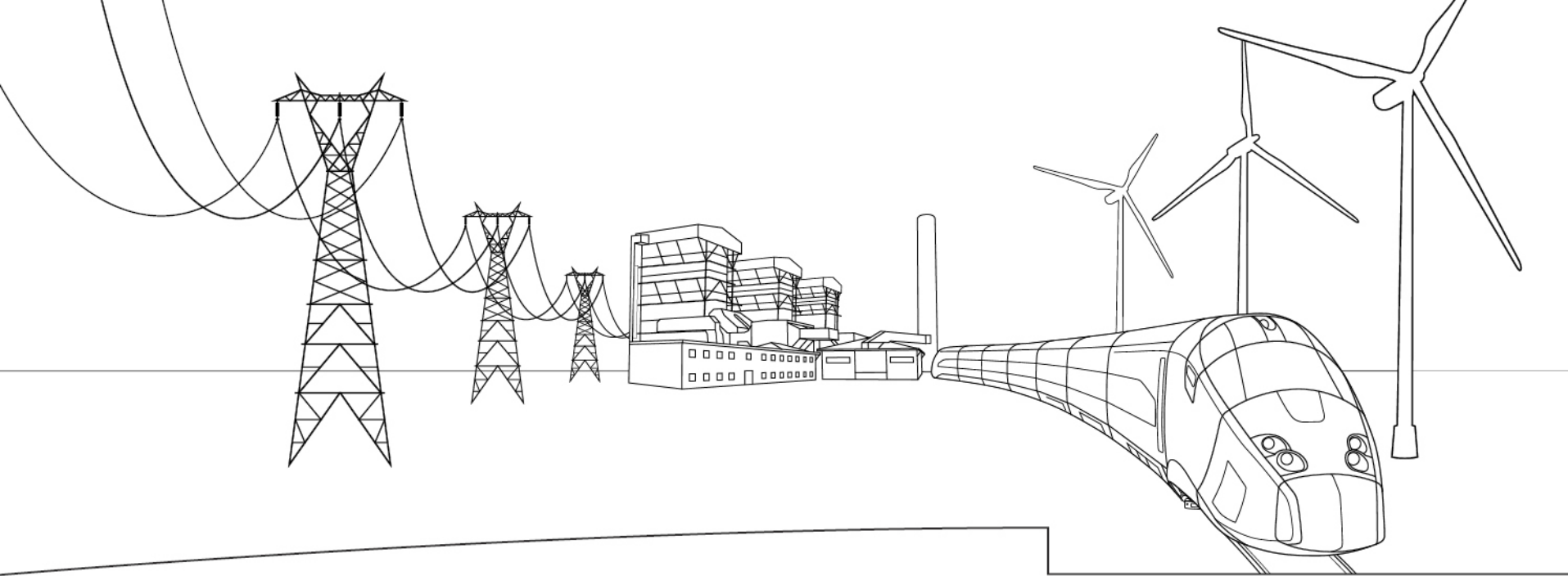
WPCA-Entergy
“Increasing Energy Efficiency of Existing Units” Seminar
January 22, 2014

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Ways to Increase Boiler & Auxiliary Equipment Efficiency

Danny Gelbar

Manager of Performance Design Engineering

The Woodland, Texas

1/22/14

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Shaping the future

Items To Be Covered

- **Boiler Efficiency Improvements**
- **Auxiliary Equipment Improvements**
- **Repowering of Existing Boilers**
- **Optimize Plant Retrofit**

Boiler Efficiency Improvements

Increase Boiler Efficiency – 1/22/14

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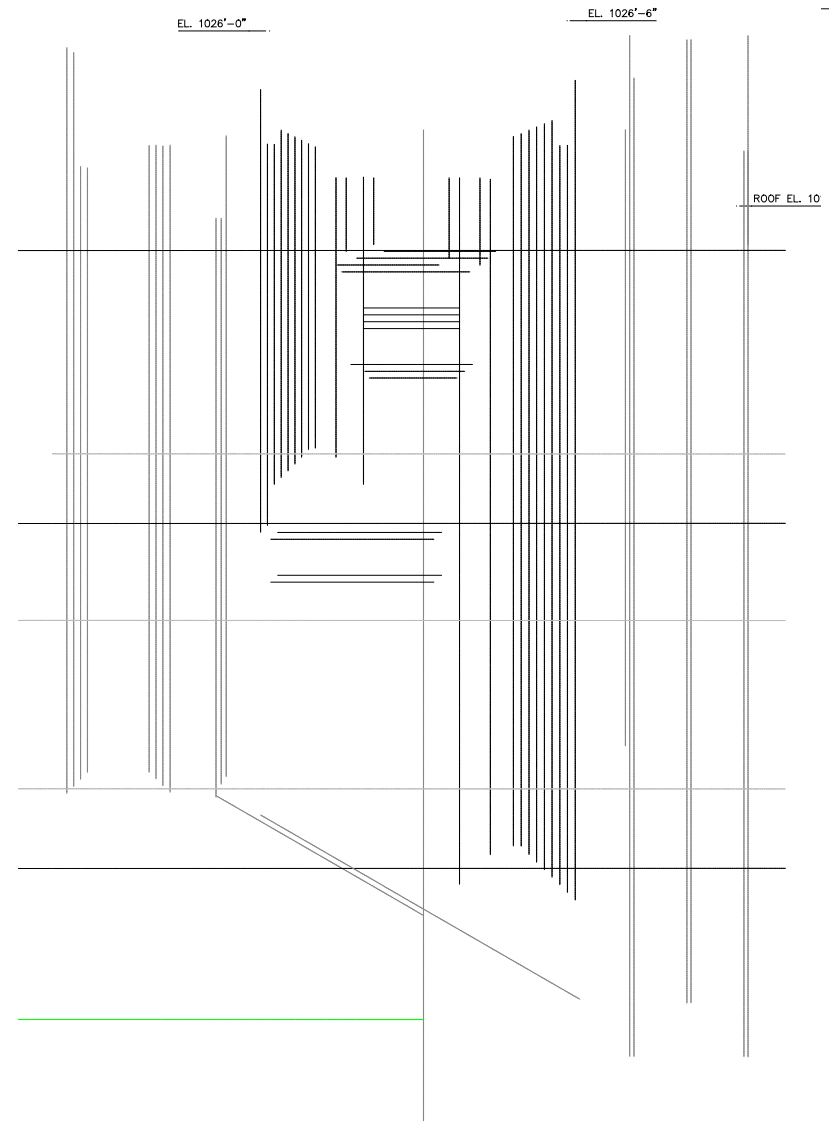
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Superheater, Reheater & Economizer

- SH & RH Steam Temperatures
- SH Desuperheater
- RH Desuperheater
- Economizer Redesign
- Reduce Sections Draft Losses
- RH Steam Side Pressure Drop (Normally about 30 psi)

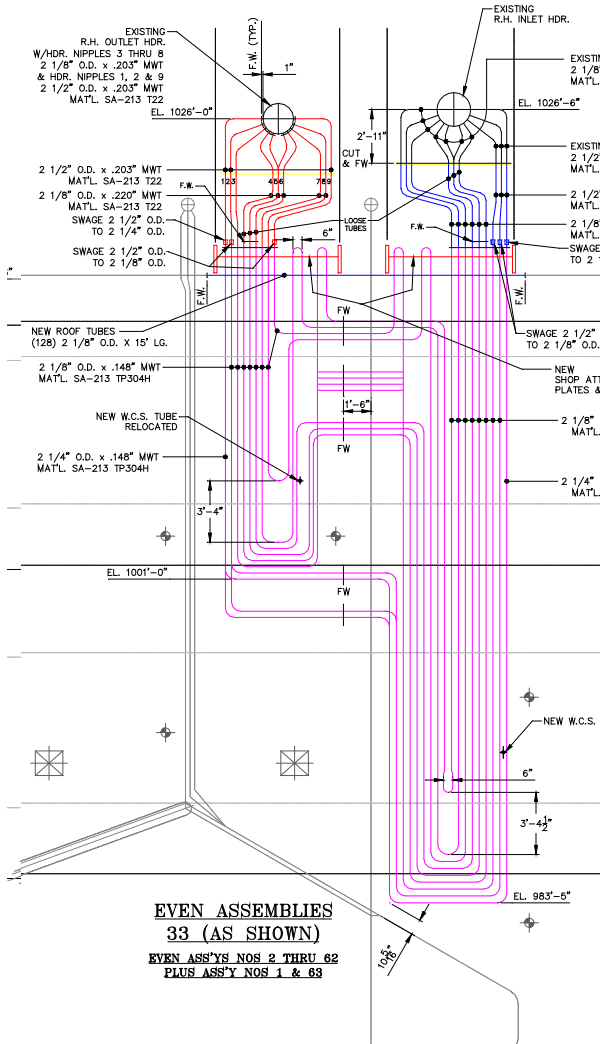
Existing 400 MW Boiler

- Plugging of Lower Portion of Front RH Pendant
- Tight 9" Spacing between RH Assemblies



Modified 400 MW Boiler

- Installed Short and Long Front and Rear Alternating Pendants



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Superheat Steam Temperature Increase

PARAMETRIC VARIABLES

1.60 Fuel Cost \$/Million BTU

600 Generator Output MW

80.00 Capacity Factor Percent

10,200 Assumed Net Unit Heat Rate - Btu/KWhr

1,005 New SH Steam Temperature - deg.F

985 Present SH Steam Temperature - deg.F

**Yearly Fuel
\$ Savings**

\$188,375

*Calculations are based on 1986 EPRI
Report CS-4554 on "Heat
Rate Improvements Guidelines for
Existing Fossil Plants"*

-28.00 Btu/kWh Effect on Heat Rate

0.27% Change in Heat Rate

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Reheat Steam Temperature Increase

PARAMETRIC VARIABLES

1.60 Fuel Cost \$/Million BTU

600 Generator Output MW

80.00 Capacity Factor Percent

10,200 Assumed Net Unit Heat Rate - Btu/KWhr

1,005 New RH Steam Temperature - deg.F

980 Present RH Steam Temperature - deg.F

**Yearly
\$ Savings**

\$218,650

*Calculations are based on 1986
EPRI Report CS-4554 on "Heat
Rate Improvements Guidelines for
Existing Fossil Plants"*

-32.50 Btu/kWh Effect on Heat Rate

0.32% Change in Heat Rate

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Superheat Desuperheater Spray Flow Reduction

PARAMETRIC VARIABLES

1.60 Fuel Cost \$/Million BTU

600 Generator Output MW

80.00 Capacity Factor Percent

10,200 Assumed Net Unit Heat Rate - Btu/KWhr

0 New Spray Flow - lbs/hr

204,000 Present Spray Flow - lbs/hr

4,080,000 Main Steam Flow - lbs/hr

-14.28 Btu/kWh Effect on Heat Rate

0.14% Change in Heat Rate

**Yearly Fuel
\$ Savings**

\$96,071

*Calculations are based on 1986
EPRI Report CS-4554 on "Heat
Rate Improvements Guidelines
for Existing Fossil Plants"*

Reheat Desuperheater Spray Flow Reduction

PARAMETRIC VARIABLES

1.60 Fuel Cost \$/Million BTU

600 Generator Output MW

80.00 Capacity Factor Percent

10,200 Assumed Net Unit Heat Rate - Btu/KWhr

0 New Spray Flow - lbs/hr

188,550 Present Spray Flow - lbs/hr

3,771,000 Cold Reheat Steam Flow - lbs/hr

-102.00 Btu/kWh Effect on Heat Rate

1.00% Change in Heat Rate

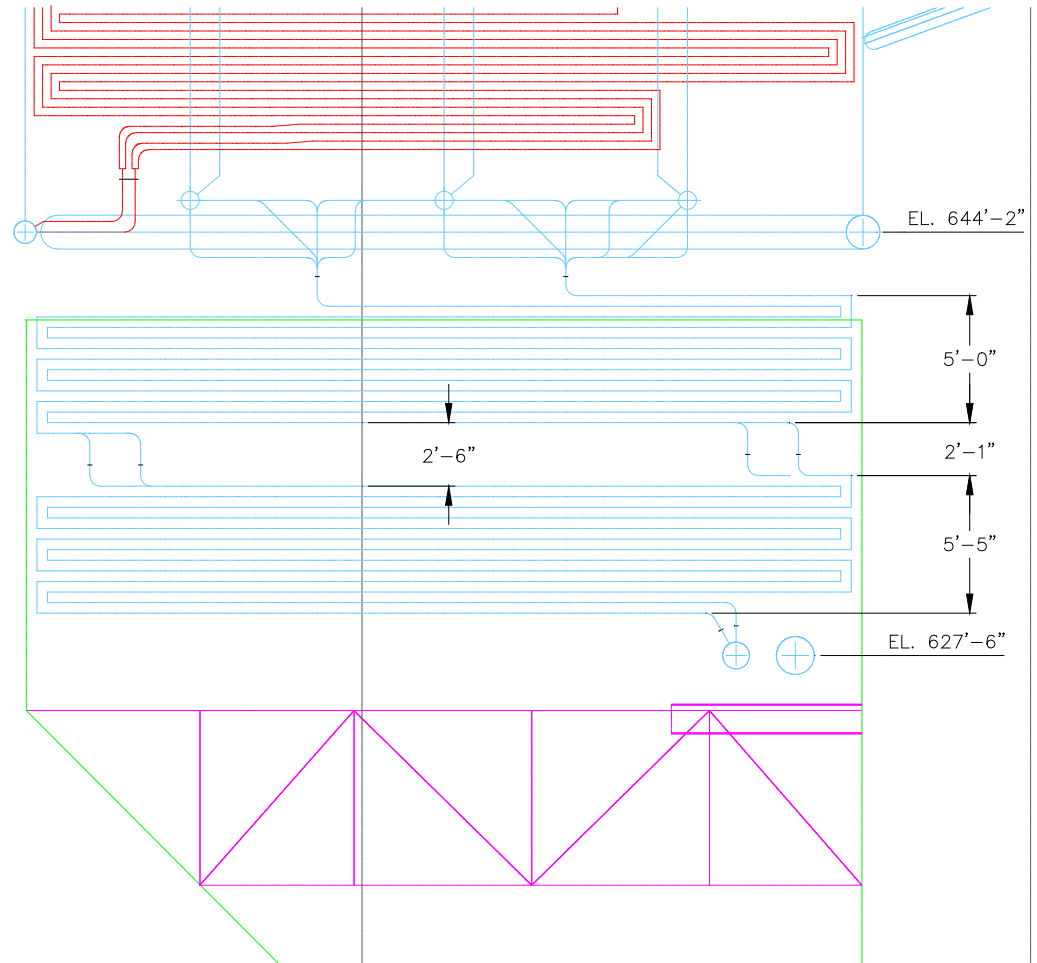
**Yearly
\$ Savings**

\$686,223

*Calculations are based on 1986 EPRI
Report CS-4554 on "Heat
Rate Improvements Guidelines for
Existing Fossil Plants"*

Existing 600 MW Boiler

- Replacement Two Bank CFS Economizer
- Plugging and Fouling Were Major Problems
- High Draft Loss Limited The Maximum Load
- High Exit Gas Temp

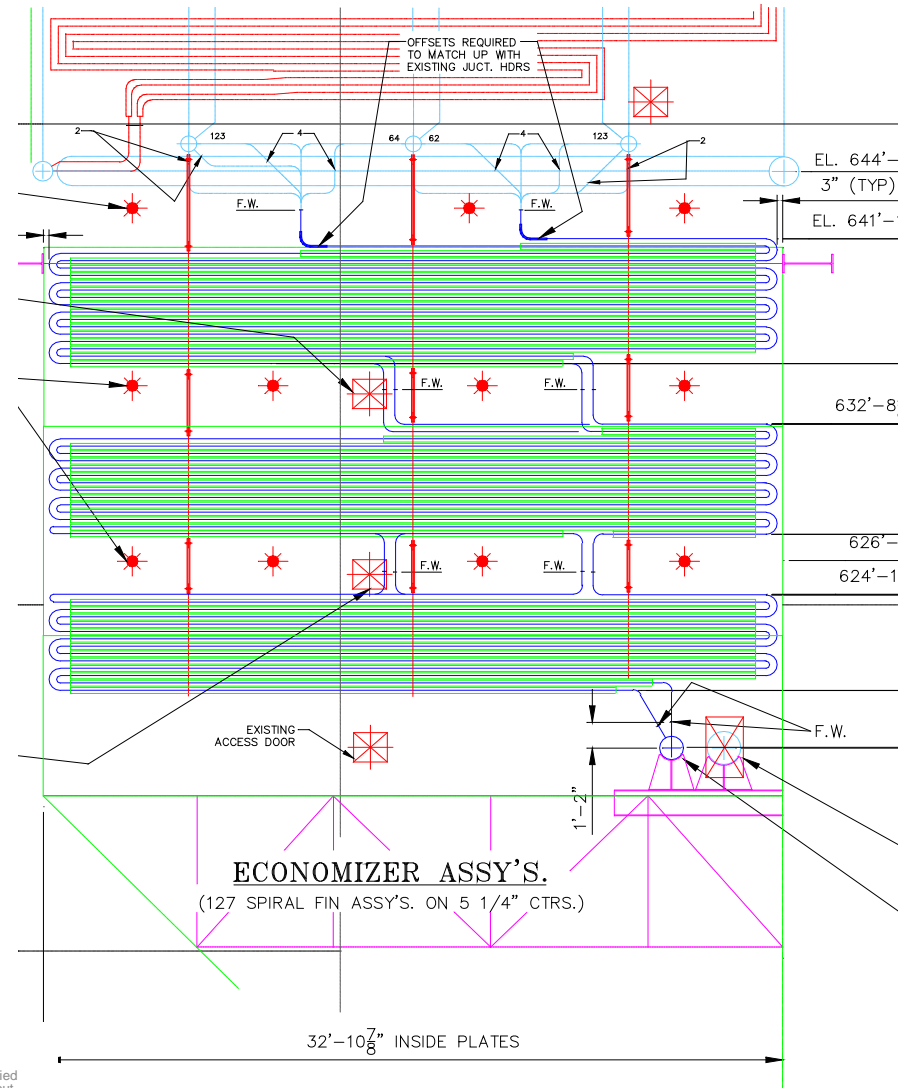


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Economizer Modifications

- In-Line SFS Economizer Installed to Reduce Plugging
- In-Line Arrangement Allows for Improved Cleaning/Sootblowing
- Reduced Draft Loss 60%, no ID fan load limitation
- Maintain or lower economizer exit gas temperature, which improves Boiler Efficiency by 1%



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Boiler Efficiency Change with Economizer Modifications

PARAMETRIC VARIABLES

1.60 Fuel Cost \$/Million BTU

600 Generator Output MW

80.00 Capacity Factor Percent

3.00 Yearly Fuel Inflation Percent

5 Year Evaluation Period

10,200 Assumed Net Unit Heat Rate - Btu/KWhr

84.50 Original Boiler Efficiency

85.50 New Boiler Efficiency

-119.30 Btu/kWh Effect on Heat Rate

-1.17% Change in Heat Rate

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Yearly
\$ Savings
\$802,600

*Calculations are based on 1986
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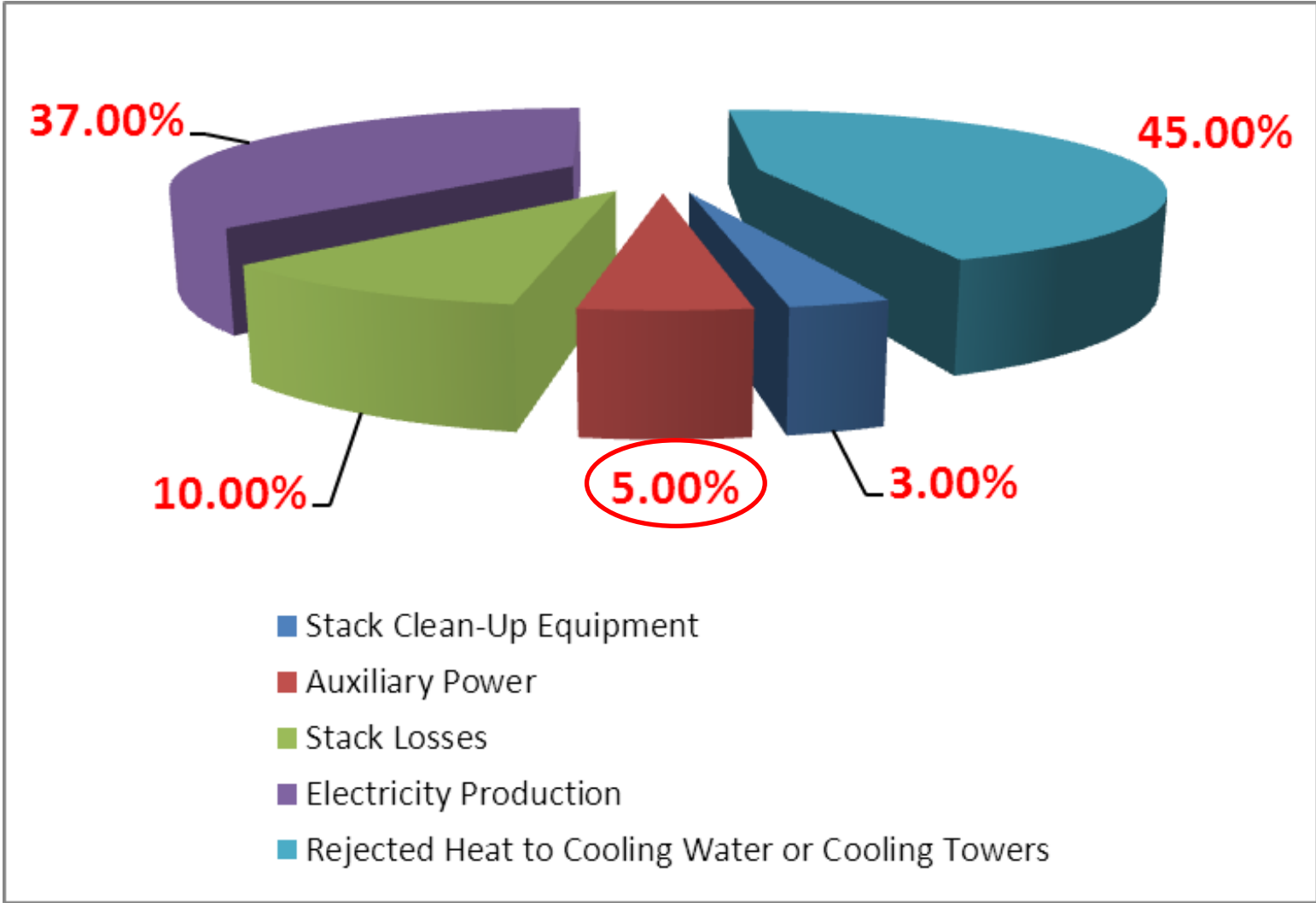
Auxiliary Equipment Improvements

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Auxiliary Equipment Improvements



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Auxiliary Equipment Improvements

- **Force Draft Fans**
- **Induce Draft Fans**
- **Primary Air Fans**
- **Pulverizers**
- **Boiler Water Circulation Pumps**

Force Draft Fans

- **Reduce Air Flow by:**
 - Decreasing Excess Air
 - Reduce Air Preheater Air Leakage
- **Reduce Air Side Losses**
 - Install Turning Vanes
 - Redesign Ductwork
 - Adjust Windbox Delta Pressure
 - Chance Out AH Baskets

Induce Draft Fans

- **Reduce Gas Flow by:**
 - Decreasing Excess Air
 - Lower Gas Temperature
 - Reduce Air Preheater Air Leakage
- **Reduce Gas Side Losses**
 - Install Turning Vanes
 - Redesign Ductwork
 - Chance Out AH Baskets

Primary Air Fans

- **Reduce Air Flow by:**
 - Reducing AH Air Leakage
 - Lower Air by taking a Pulverizer Out of Service
- **Reduce Air Side Losses**
 - Install Turning Vanes
 - Redesign Ductwork
 - Change Out AH Baskets
 - Change Out Coal Piping

Pulverizers

- **Reduce the Number of Pulverizers in Service**
- **Change the Coal Being Fired with One that has a higher Hardgrove Grindability and lower Moisture Content or Change the Coal Fineness Leaving**
- **Increase the pulverizer outlet temperature which raises the air flow through the Air Preheater. The affect on Boiler Efficiency can increase by up to 0.5%.**
- **Install More Efficient Motors**

Boiler Water Circulation Pumps

- **Take one of the of the Boiler Water Circulation Pumps out of service if permitted by OEM.**
 - **Most Controlled Circulation Boiler were designed with 4 out of 4 pumps in service at MCR. The OEM can evaluate the waterwall circulation system to determine if the unit can operate with 3 out of 4 pumps in service**

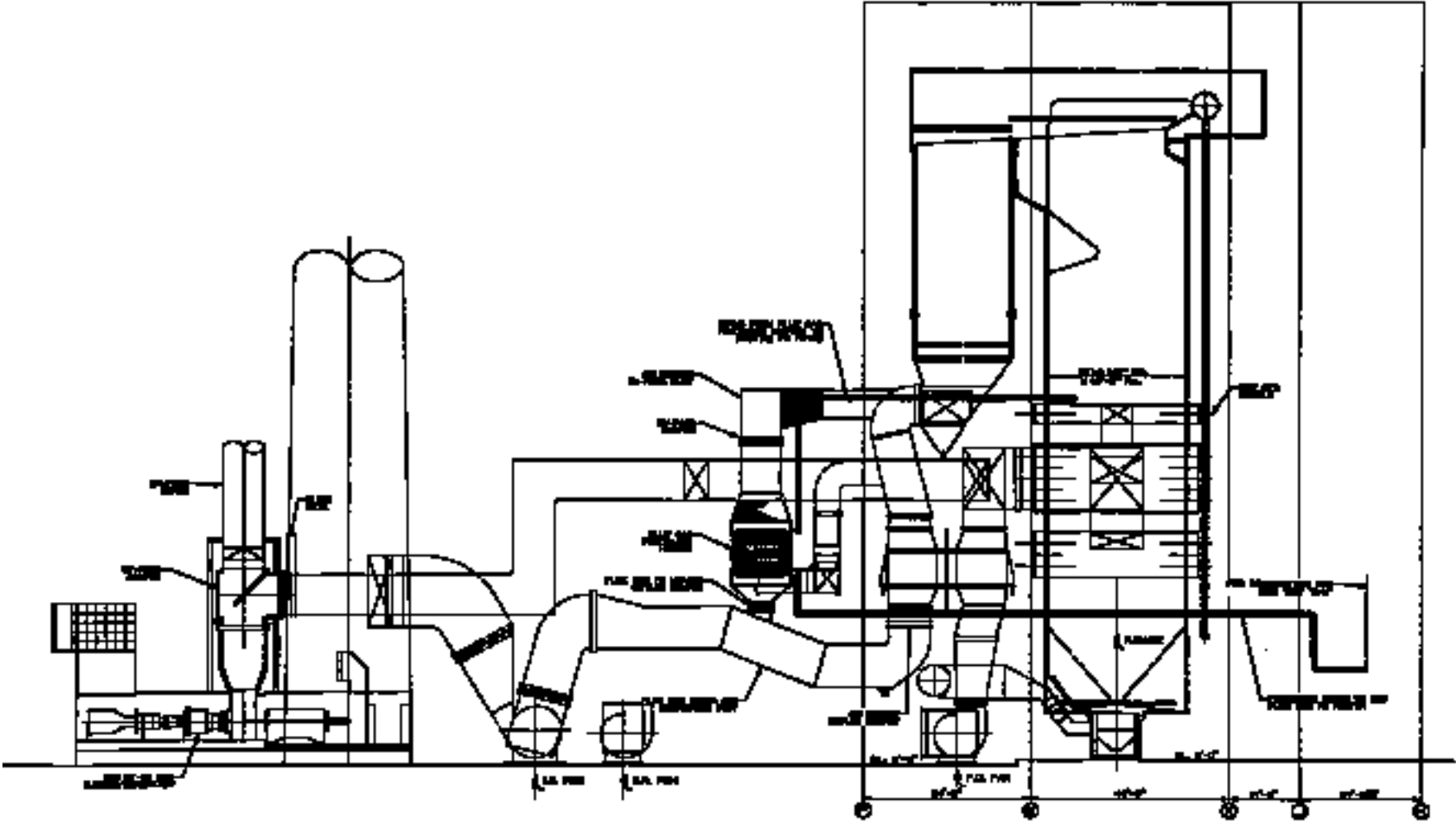
Repowering of Existing Boiler

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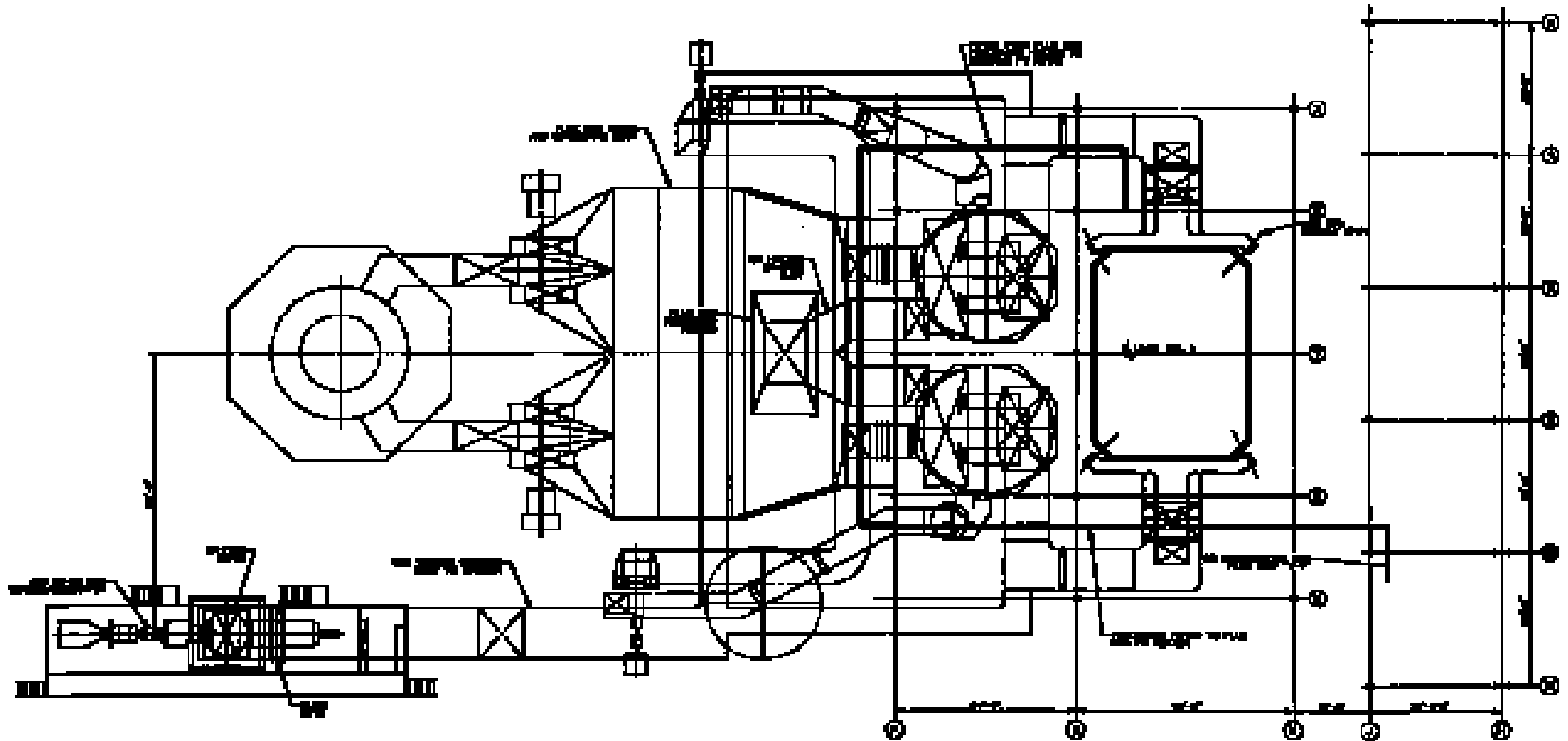
Hot Windbox Repowering



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Hot Windbox Repowering



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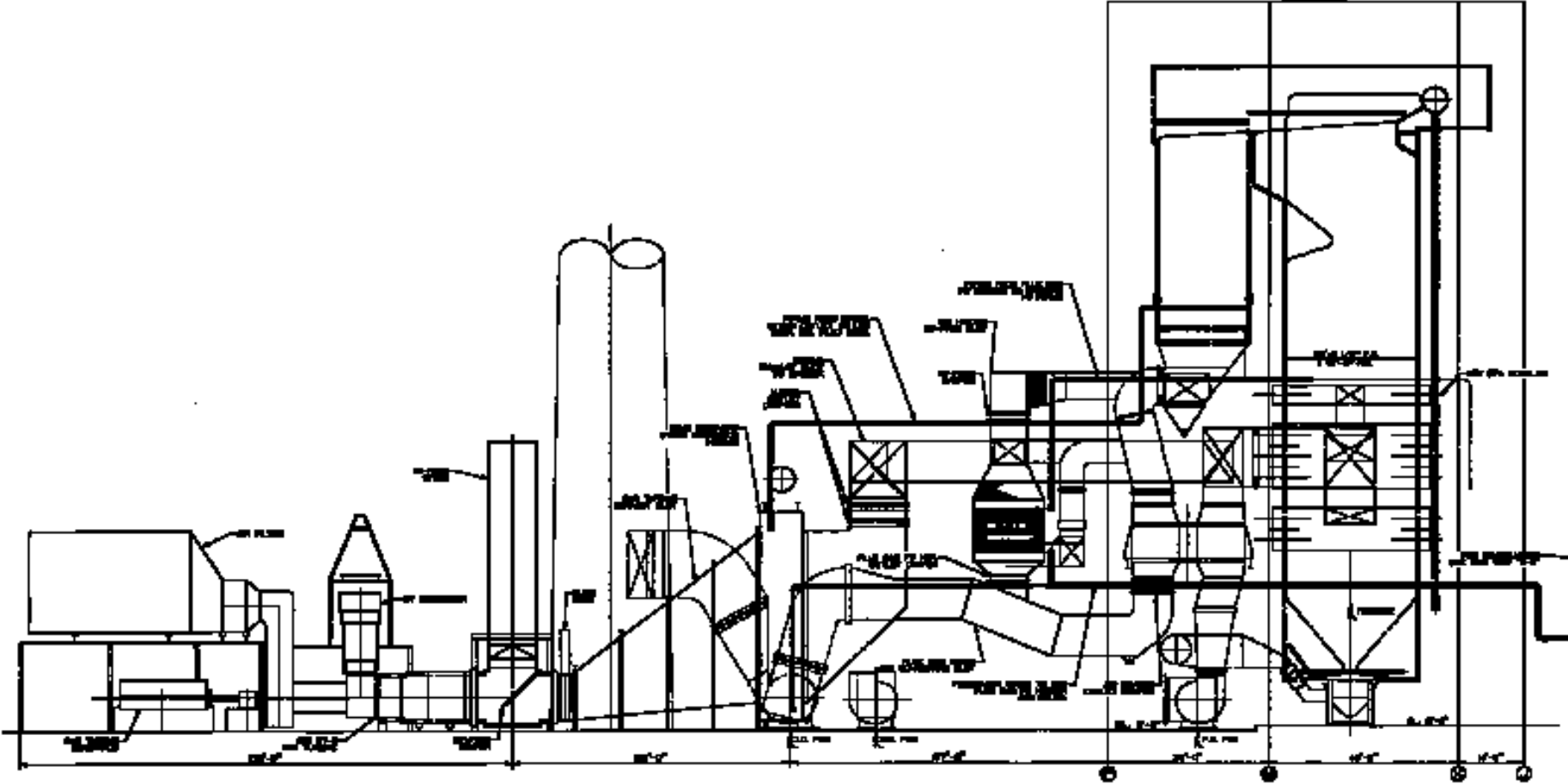
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Hot Windbox Repowering

- If the boiler/turbine cycle normally puts out 200 MWs, the combustion turbine can only be about 65 MWs in size. The limitations are the following:
 - The combustion turbine exhaust is normally in the 900 degF to 1200 degF.
 - Mixed air temperature to the windbox can not exceed 800 degF since the ductwork and windbox are made of carbon steel.
 - The boiler will not be able to achieve full load, so the total MWs will only increase by 10%.
 - Must evaluate I.D, Fans capacity. However, the F.D. Fans will have lower required duty.
 - The improvement in Plant Heat Rate is in the 2% - 3% range.

Cold Windbox Repowering

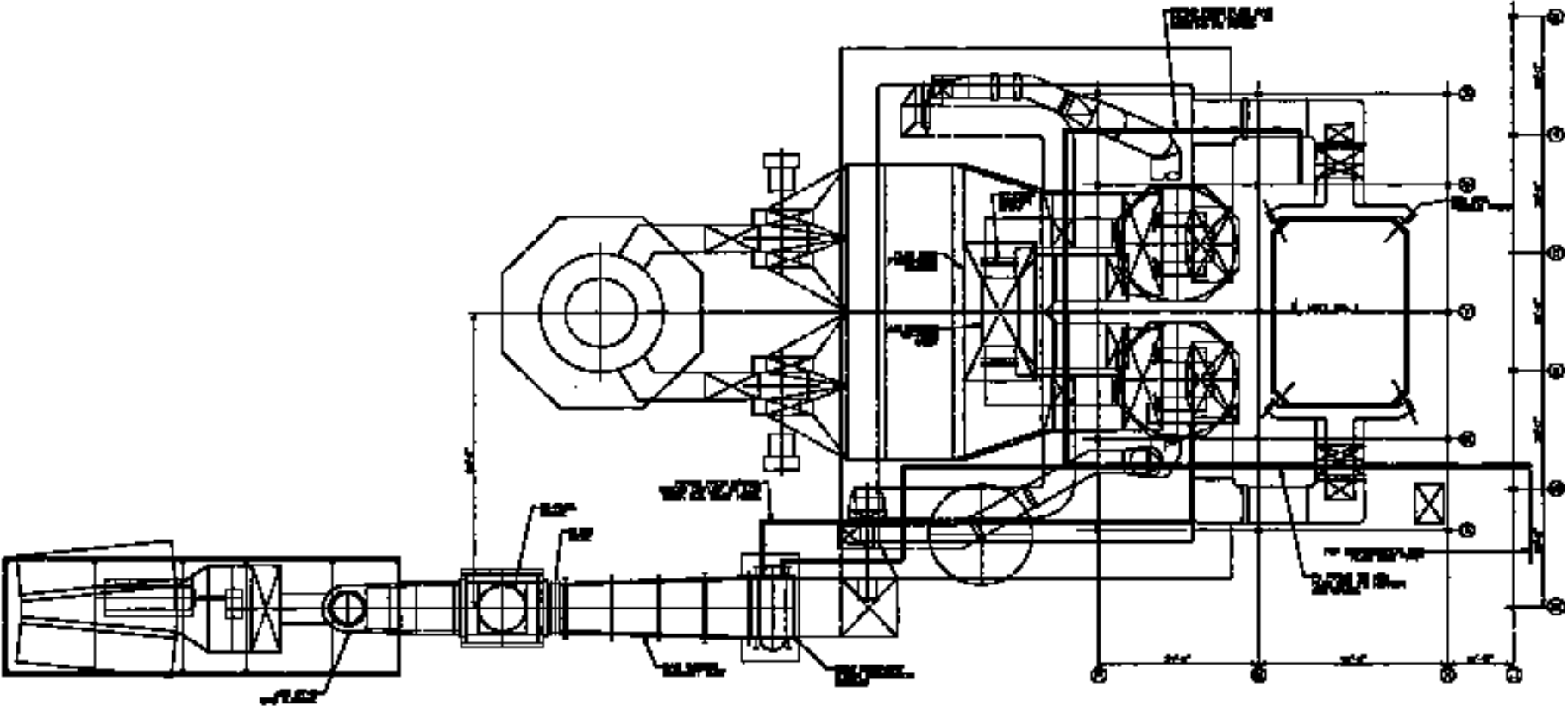


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Cold Windbox Repowering



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Cold Windbox Repowering

- If the boiler/turbine cycle normally puts out 200 MWs, the combustion turbine can only be about 100 MWs in size. The limitations are the following:
 - The combustion turbine exhaust is normally in the 1000 degF to 1200 degF. This flow will be cooled down to 750 degF by a small HRSG.
 - Mixed air temperature to the windbox will be below 750 degF .
 - The boiler will not be able to achieve full load, so the total MWs will only increase by 30%.
 - Must evaluate I.D, Fans capacity. However, the F.D. Fans will have lower required duty.
 - The improvement in Plant Heat Rate is in the 4% - 6% range.

Optimize Plant Retrofit

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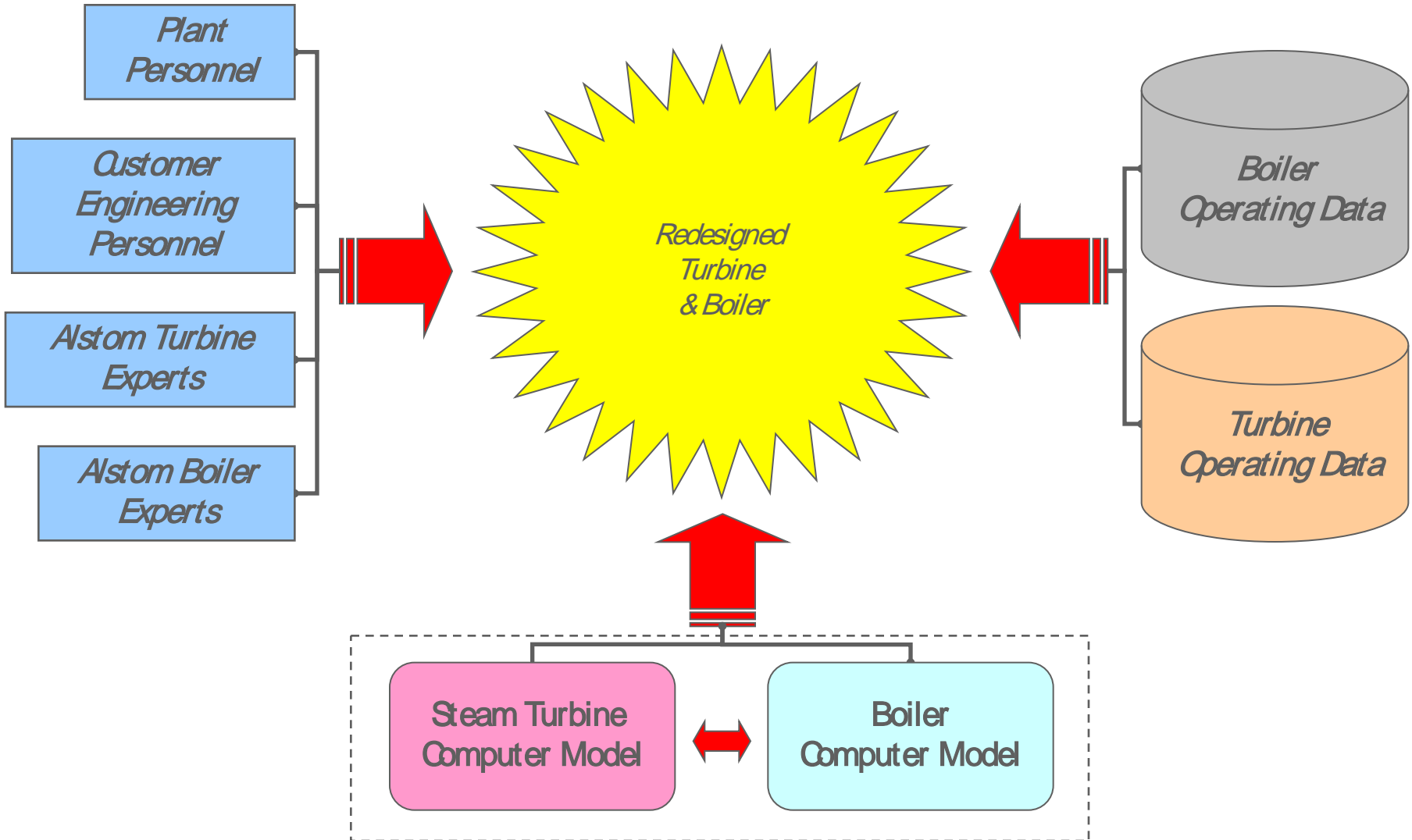
Joint Project Team Review Sessions

- **Joint Project Team Review Sessions (JPTR)** are an essential part of the OPR concept **unique** to Alstom
- Structured to afford the Customer an opportunity to participate with Alstom specialists in an **interactive** engineering design session
- Allow the Customer **and** Alstom to quickly work through a number of various options



- JPTR session is followed up by more detailed thermodynamic work, hardware selection and costing

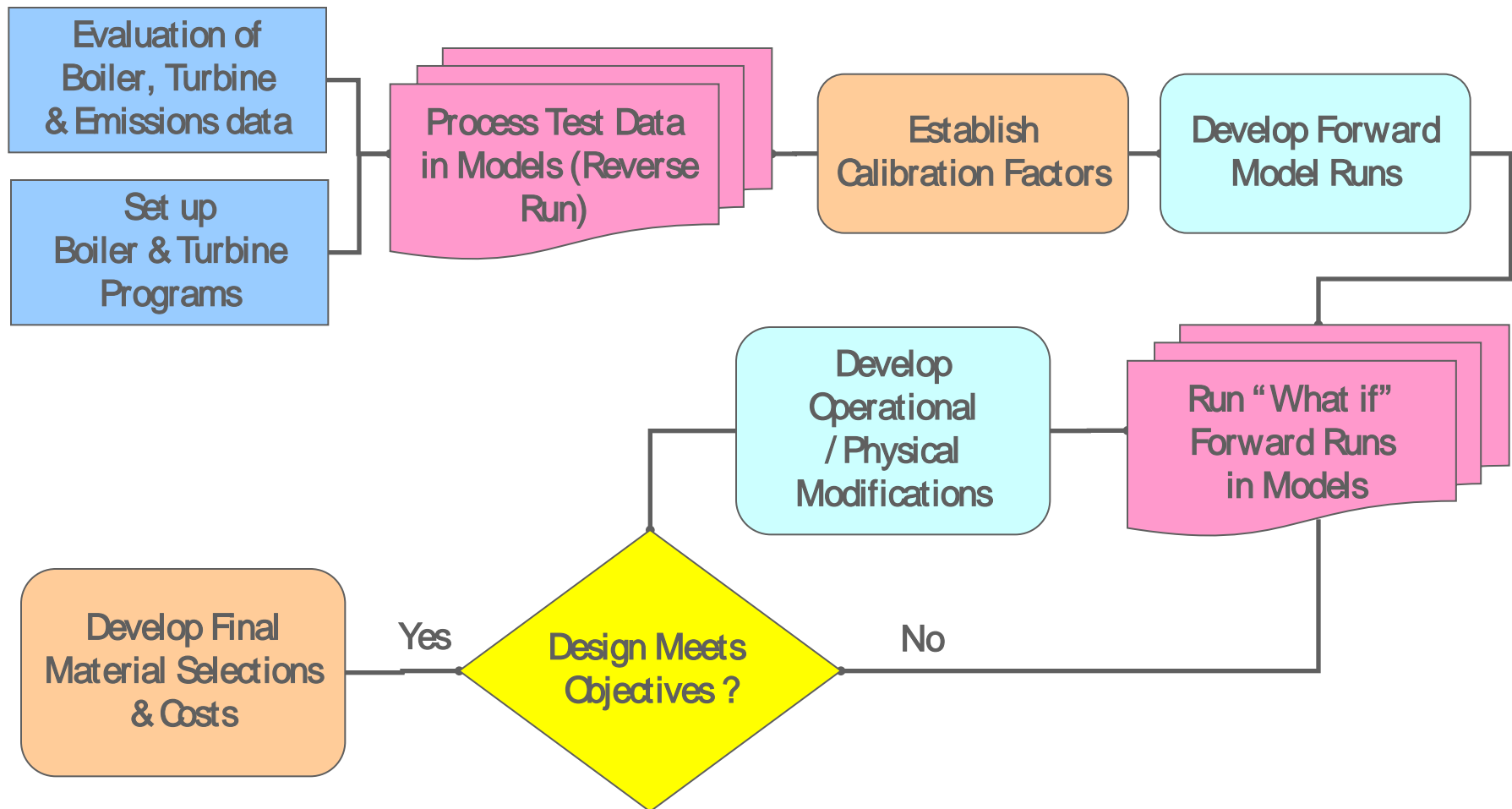
Joint Project Team Design Process



Increase Boiler Efficiency – 1/22/14

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Joint Project Team Design Process

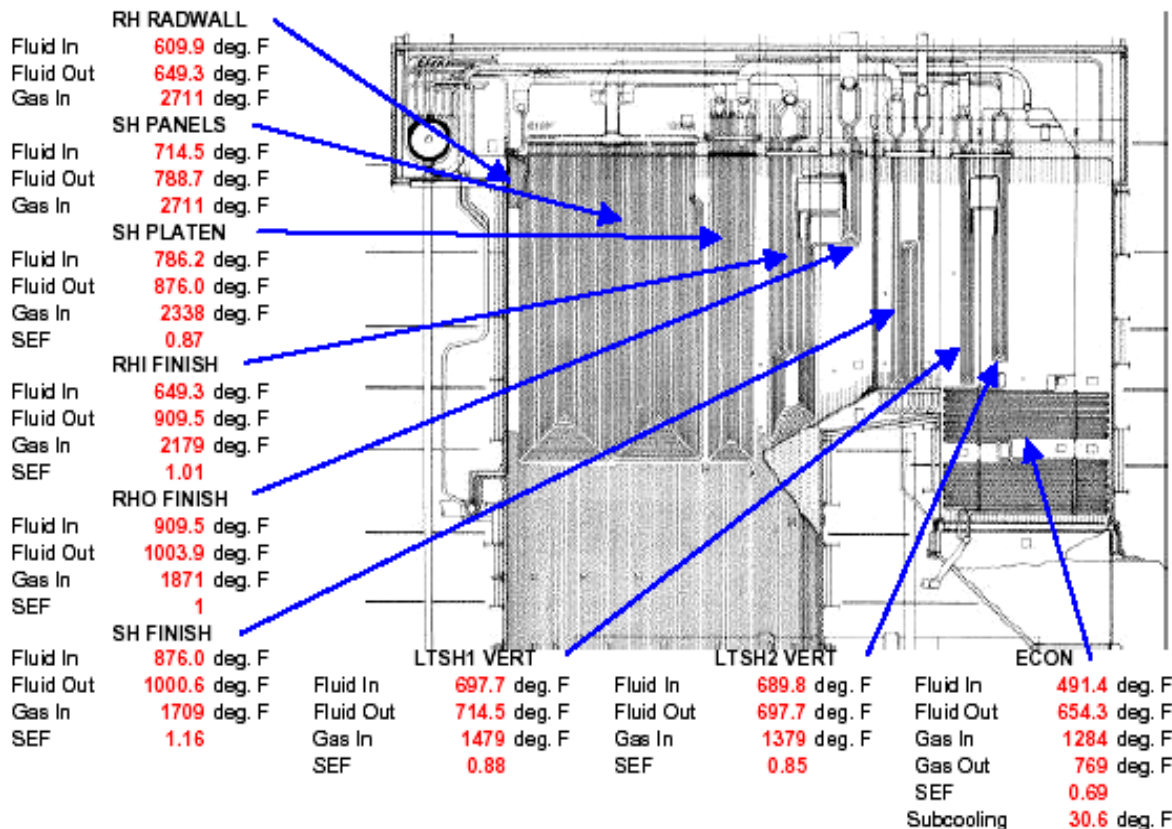


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JPTDR Boiler & Turbine Model Results

Run No. 21 Run Type Same as Run 20 (with new Steam Turbine Condition with RH Finishing on 9.5" centers - platenized & New In-Line SFS Econ) but running Steam Turbine at 2470psig Throttle pressure and increase main steam flow and 6 mill in Service



General Performance Information

SH Steam Flow	3,935,613 lbs/hr
RH Steam Flow	3,535,221 lbs/hr
SHO Temp	1001.0 °F
SH Desup Spray	0.30 %
RH Desup Spray	1.10 %
SHDesuperheater Spray	11263 lbs/hr
RHDesuperheater Spray	39359 lbs/hr
RHO Temp	1004.0 °F
RHDESUP OUT TMP	610.0 °F
Feedwater Temp	491.0 °F
Econ Exit Gas Temp	769.0 °F
AH TGO Uncorr	320.0 °F
AH TGO Corr	306.0 °F
Tilt	-11 degrees
Excess Air	26 %
Fuel Fired	618,334 lbs/hr
Boiler Efficiency	85.45 %
NHI/PA	2.08 Mbtu/hr-ft2

Steam Turbine Performance

Output	571,060 KWs
Turbine Heat Rate	8,128 BTU/KW-hr
Superheater Outlet Flow	3,935,613 lbs/hr
Main Steam Temp.	1,000 °F
Throttle Pressure	2,470 psia
Cold RH Flow	3,495,862 lbs/hr
Cold RH Pressure	638 psia
Cold RH Temp.	633 °F
Hot RH Flow	3,531,173 lbs/hr
Hot RH Pressure	569 psia
Hot RH Temp.	1,000 °F
Reheater Spray Flow	35,312 lbs/hr
Main Condenser Pressure	1.8 psia

Mill Performance

Air In Per Mill	197,938 lbs/hr	Outlet Moisture	15.66 %
COAL FLOW PER MILL	103,056 lbs/hr	Hot Air Temperature Required	569.6 °F
NO. MILLS IN SERVICE	6 OF 6	TEMPERING AIR TEMP.	82 °F
Grinding Capacity	79.1 %	AVAILABLE HOT AIR TEMP.	691 °F
MIXTURE TEMPERATURE	146 °F		

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OPR Example

- HP/IP turbine retrofit ~ 5% MW improvement
- Division panel redesign reduced tube failures, improved gas flow distribution
- Larger economizer, wider gas path, improved heat rate, $\Delta P \downarrow$, Fan HP \downarrow
- Economizer Exit gas temp \downarrow Precip. efficiency \uparrow
- Improve boiler cleanliness w/ water cannons
- Improved access for maintenance
- Replaced AH - 48 vs. 408 baskets,
 - Gas side $\Delta P \downarrow$, Fan HP \downarrow

24-27MW

15-18MW

Total Net Unit Output Increase

40- 45MW



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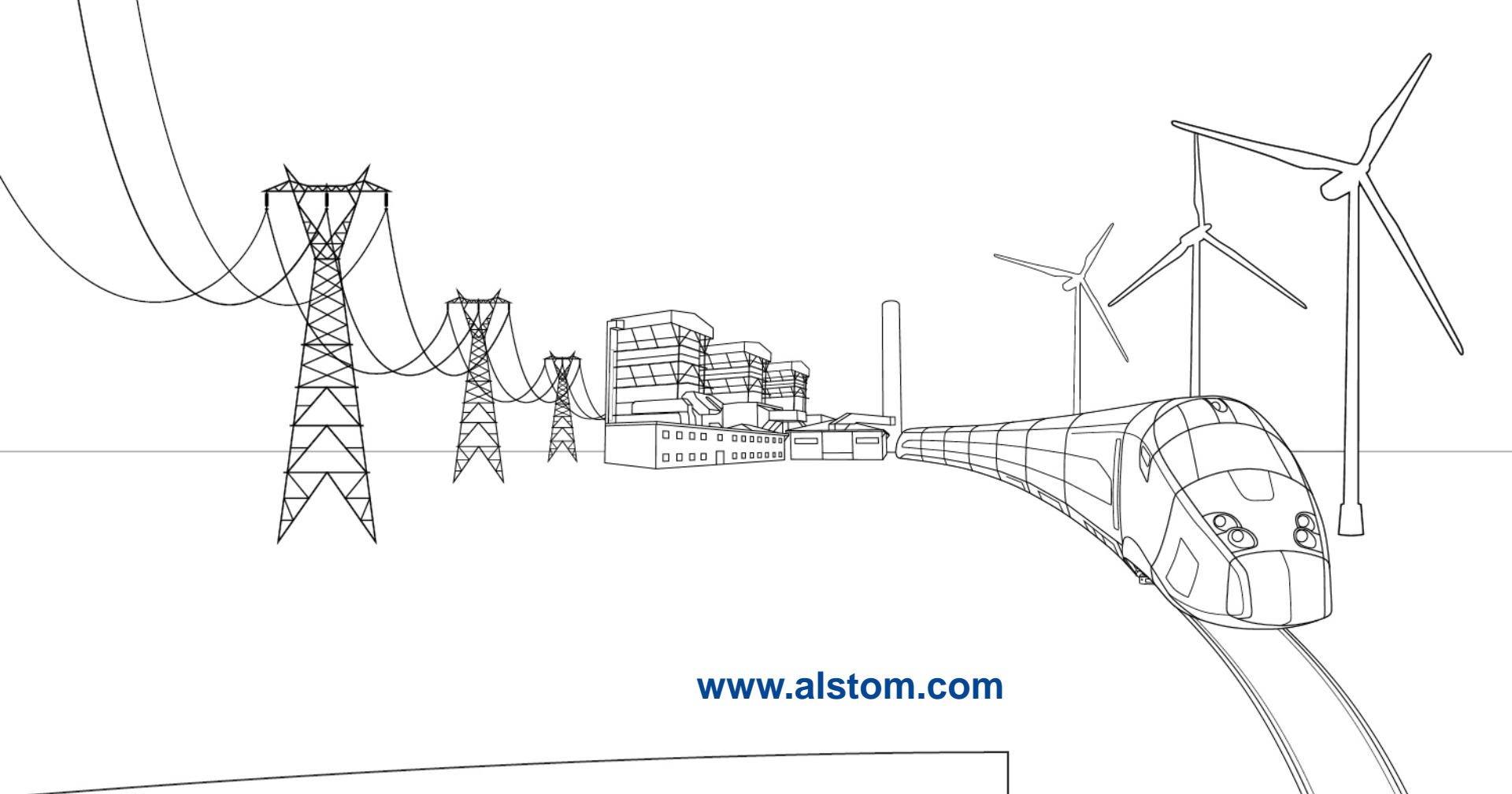
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Questions

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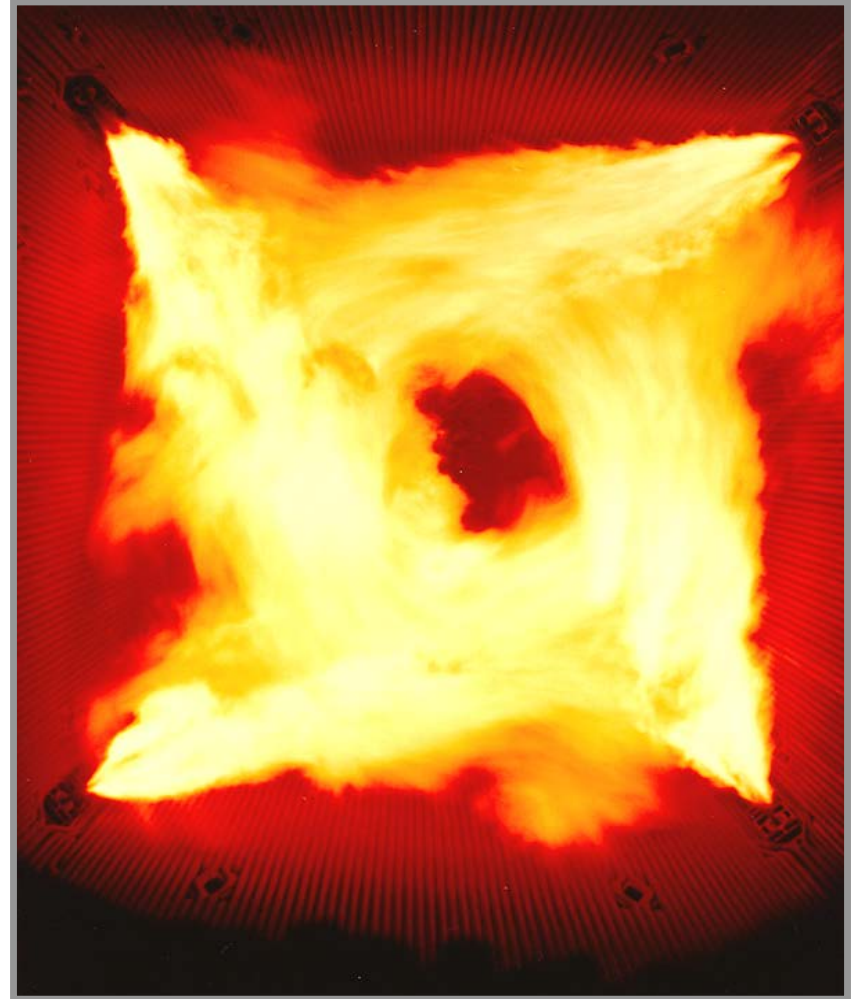


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Tangential Firing System

- Flame Pattern of Tangential Firing System



Superheater & Reheater Components

Boiler Efficiency Effects on Heat Rate

PARAMETRIC VARIABLES

1.60 Fuel Cost \$/Million BTU

600 Generator Output MW

80.00 Capacity Factor Percent

10,200 Assumed Net Unit Heat Rate - Btu/KWhr

89.33 Present Boiler Efficiency

89.25 New Boiler Efficiency

9.14 Btu/kWh Effect on Heat Rate

-0.09% Change in Heat Rate

Yearly Fuel
\$ Savings

(\$61,510)

*Calculations are based on 1986
EPRI Report CS-4554 on "Heat
Rate Improvements Guidelines for
Existing Fossil Plants"*